



Date: April 3, 1992

To: Michael Hills, Permit Section, DAPC

From: Frederick L. Smith 1

Subject: Meyer Steel Drum, Inc.: Chicago: Stack Test Evaluation:
Drum Reclamation Process with Afterburner Control:
031-600 APY: 91040073 MYERTEST.VOC

RECEIVED

708/531-5900

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ENVIRONMENTAL PROTECTION AGENCY
DIVISION OF PERMITS
STATE OF ILLINOIS

Meyer Steel Drum, Inc. retained Williams & Wentink as their environmental consultant, who in turn contracted with Mostardi-Platt to conduct VOC and particulate matter emissions from a new Drum Reclamation a process which is controlled by a thermal afterburner. The testing was conducted on December 12 & 13, 1991. Four tests were conducted. Test number 1 was not acceptable to the Agency due to higher than normal incinerator operating conditions. A fourth test was run and a total of three tests (Nos. 2-4) were submitted in the final report to demonstrate compliance.

Method 25 was employed to measure the VOC emissions after the thermal afterburner control. The procedure measures total gaseous non-methane organics. The particulate matter content of the exhaust gas stream was determined using Methods 1-5. Opacity of the exhaust stack was measured using Method 9.

The process includes a Winterbrother Furnace DRF-1 equipped with a waste heat boiler. The control device is a thermal afterburner which is gas fired. A total of 1335 drums were fed into the process during the three test runs. This calculates to 373 drums/hour. Each drum is estimated to weigh 43 pounds and the average residue per drum is 4.4 pounds. This works out to be a process weight rate of 17680 pounds/hour. The allowable particulate matter emissions are contained in Rule 212.321. VOC emissions are subject to Rule 218.301 which limits the organic emissions to 8 pounds/hour. The opacity readings observed during testing should be below 20 %.

Emission levels found during the testing and reported in the final report are as follows:

	Test 2	Test 3	Test 4
VOC Emissions: lbs/hr	2.50	3.21	2.49
Particulate Matter Emissions: lbs/hr	2.45	3.23	2.85
Allowable VOC: lbs/hr	8.0	8.0	8.0
Allowable Particulate: lbs/hr	7.59	8.47	8.13

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An analysis of the particulate matter emissions is attached. The values compare favorably with the results contained in the final report. VOC calculations were carried out in a proper fashion. Sampling appears to have been done according to the procedures in 40 CFR 60, Appendix A. Also, the opacity readings noted during the testing are within limits and the afterburner was operated at 1400-1600F during sampling. The ash generated goes to a landfill. It is recommended the results contained in the final report be accepted as valid.

c.c. Miles Zamco: FOS Springfield
Cesary Krzymowski: Region 1
Lawrence Eastep: DLPC



**MOSTARDI-PLATT
ASSOCIATES, INC.**

**Meyer Steel Drum, Inc.
Method 25 - TGNMO Results Summary
Afterburner Stack
December 12 and 13, 1991**

Test No.	Date	Time	Air Flow (DSCFM)	Temp. (°F)	TGNMO Concentration (mg/m ³)	TGNMO Concentration (lbs/hr)
2	12/12/91	1315-1415	31,755	554.5	21	2.50
3	12/12/91	1500-1600	31,806	558.6	27	3.21
4	12/13/91	0730-0830	31,704	541.3	21	2.49
Average			31,755	551.5	23	2.73

$$\text{Emission Rate (lbs/hr)} = \frac{\text{TGNMO Conc. (mg/m}^3\text{)}}{1000 \text{ (l/m}^3\text{)}} \times \frac{6.24 \times 10^{-5} \text{ lbs/dscf}}{\text{mg/l}} \times \text{DSCFM} \times 60 \frac{\text{min}}{\text{hr.}}$$



PARTICULATE TEST RESULTS SUMMARY				
Plant: Meyer Steel Drum, Inc.		Source: Afterburner Stack		
Test Run Number	2	3	4	Average
Test Location	Stack	Stack	Stack	
Source Condition	Normal	Normal	Normal	
Date	12/12/91	12/12/91	12/13/91	
Time	1300-1424	1500-1605	0729-0835	
Particulate Concentration:				
@ Flue Conditions, grains/acf	0.0043	0.0056	0.0051	0.0050
@ Standard Conditions, grains/dscf	0.0090	0.0118	0.0105	0.0104
Emission Rate:				
pounds/hour	2.45	3.23	2.85	2.84
Average Gas Volumetric Flow Rate:				
@ Flue Conditions, acfm	66,182	67,185	65,005	66,124
@ Standard Conditions, dscfm	31,755	31,806	31,704	31,755
Average Gas Temperature, °F	554.5	558.6	541.3	551.5
Average Gas Velocity, ft/sec	63.85	64.82	62.71	63.79
Flue Gas Moisture, percent by volume	5.64	6.52	5.72	5.96
Average Flue Pressure, in. Hg	29.23	29.23	29.35	
Barometric Pressure, in. Hg	29.23	29.23	29.35	
Average %CO₂, by volume, dry basis	1.60	2.10	1.90	
Average %O₂, by volume, dry basis	19.00	18.40	18.40	
Dry Molecular Wt. of Gas, lb/lb-mole	29.016	29.072	29.040	
Gas Sample Volume, dscf	45.539	36.657	38.513	
Isokinetic Variance	1.01	1.02	1.03	

FLSPART

Company Name: Meyer Steel Drum

Location: Chicago

Test Number: 2

Test Date: 12/12/91

Source: Drum Reclamation Process Controlled by an Afterburner

Identification Number: 031 600 APY

Application Number: 91040073

PARTICULATE MATTER TEST

Concentration & Pollutant Mass Rate

$$Vwc = V1 \times 0.04707$$

$$Vwc = 57.8 \times 0.04707$$

$$Vwc = 2.72 \text{ scf}$$

$$VmStd = Y \times Vm \times (TsStd/Tm) \times (Pb + DH/13.6)/PsStd$$

$$VmStd = 1.012 \times 46.63 \times (528/536.6) \times (29.23 + 1.663/13.6)/29.92$$

$$VmStd = 45.55 \text{ scf}$$

$$Bwo = Vwc/VmStd + Vwc$$

$$Bwo = 2.720646 / 45.55221 + 2.720646$$

$$BWO = 0.0564$$

$$\% H2O = 5.64$$

$$1-Bwo = 0.9436$$

$$Ms = Md(1-Bwo) + 18(Bwo)$$

$$Ms = 29.016 (.9436402) + 18(5.635975E-02)$$

$$Ms = 28.40$$

$$Vs = 85.48 \times Cp \times (Ts/Ps \times Ms) \text{ Sq Rt X Dp}$$

$$Vs = 85.48 \times .84 \times (1014.5 / (29.23 \times 28.39514)) \text{ Sq Rt X } .8042$$

$$Vs = 63.84 \text{ feet per second}$$

$$Qs = As \times Vs \times 60$$

$$Qs = 17.176 \times 63.84069 \times 60$$

$$Qs = 65792 \text{ acfm}$$

$QsStd = Qs \times (Ps/PsStd) \times (TsStd/Ts) \times (1-Bwo)$
 $QsStd = 65791.66 \times (29.23/29.92) \times (529/1014.5) \times (1-5.635975E-02)$
 $QsStd = 31566 \text{ scfm}$

$Cs = (Wt \times 15.43)/VmStd$
 $Cs = (.0265 \times 15.43)/45.55221$
 $Cs = 0.0090 \text{ grains/scf}$

$PMRc = (Cs \times QsStd \times 60)/7000$
 $PMRc = (8.976404E-03 \times 31566.5 \times 60)/7000$
 $PMRc = 2.4287 \text{ pounds/hour}$

$PMRa = (Wt \times As)/(Time:Hours \times An \times 454)$
 $PMRa = (.0265 \times 17.176)/(1.2 \times .000341 \times 454)$
 $PMRa = 2.4501 \text{ pounds/hour}$

$I = (PMRa/PMRc) \times 100$
 $I = (2.450058 / 2.428746) \times 100$
 $I = 100.88 \%$

$Isokinetic \text{ Rate} = (VmStd \times As)/(An \times Minutes \times QsStd) \times 100$
 $Isokinetic \text{ Rate} = (45.55221 \times 17.176)/(.000341 \times 72 \times 31566.5) \times 100$
 $Isokinetic \text{ Rate} = 100.95 \%$

Appl. No.=91040073 2

V1=57.8

Y=1.012

Vm=46.63

T1=76.6

Pb=29.23

DH=1.663

Cp=.84

T2=554.5

Ps=29.23

DP=0.8042

CO2=1.6

O2=19.0

CO=0

As=17.176

Wt=0.0265

An=.000341

Time: Minutes=72

Time:Hours=1.2

Btu=1

FO=1

FLSPART

Company Name: Meyer Steel Drum

Location: Chicago

Test Number: 3

Test Date: 12/12/91

Source: Drum Reclamation Process Controlled by an Afterburner

Identification Number: 031 600 APY

Application Number: 91040073

PARTICULATE MATTER TEST

Concentration & Pollutant Mass Rate

$$Vwc = V1 \times 0.04707$$

$$Vwc = 54.3 \times 0.04707$$

$$Vwc = 2.56 \text{ scf}$$

$$VmStd = Y \times Vm \times (TsStd/Tm) \times (Pb + DH/13.6)/PsStd$$

$$VmStd = 1.012 \times 37.87 \times (528/541.3) \times (29.23 + 1.694/13.6)/29.92$$

$$VmStd = 36.68 \text{ scf}$$

$$Bwo = Vwc/VmStd + Vwc$$

$$Bwo = 2.555901 / 36.67631 + 2.555901$$

$$BWO = 0.0651$$

$$\% H2O = 6.51$$

$$1-Rwo = 0.9349$$

$$Ms = Md(1-Bwo) + 18(Bwo)$$

$$Ms = 29.072 (.934852) + 18(6.514803E-02)$$

$$Ms = 28.35$$

$$Vs = 85.48 \times Cp \times (Ts/Ps \times Ms) \text{ Sq Rt X Dp}$$

$$Vs = 85.48 \times .84 \times (1018.6 / (29.23 \times 28.35068)) \text{ Sq Rt X .8141}$$

$$Vs = 64.81 \text{ feet per second}$$

$$Qs = As \times Vs \times 60$$

$$Qs = 17.276 \times 64.80779 \times 60$$

$$Qs = 67177 \text{ acfm}$$

$QsStd = Qs \times (Ps/PsStd) \times (TsStd/Ts) \times (1-Bwo)$
 $QsStd = 67177.16 \times (29.23/29.92) \times (529/1018.6) \times (1-6.514803E-02)$
 $QsStd = 31803 \text{ scfm}$

$Cs = (Wt \times 15.43)/VmStd$
 $Cs = (.0281 \times 15.43)/36.67631$
 $Cs = 0.0118 \text{ grains/scf}$

$PMRc = (Cs \times QsStd \times 60)/7000$
 $PMRc = (1.182188E-02 \times 31802.55 \times 60)/7000$
 $PMRc = 3.2226 \text{ pounds/hour}$

$PMRa = (Wt \times As)/(Time:Hours \times An \times 454)$
 $PMRa = (.0281 \times 17.276)/(.95833 \times .000341 \times 454)$
 $PMRa = 3.2721 \text{ pounds/hour}$

$I = (PMRa/PMRc) \times 100$
 $I = (3.272082 / 3.222566) \times 100$
 $I = 101.54 \%$

$Isokinetic \text{ Rate} = (VmStd \times As)/(An \times Minutes \times QsStd) \times 100$
 $Isokinetic \text{ Rate} = (36.67631 \times 17.276)/(.000341 \times 57.5 \times 31802.55) \times 100$
 $Isokinetic \text{ Rate} = 101.61 \%$

$Y=1.012$
 $Vm=37.87$
 $T1=81.3$
 $Pb=29.23$
 $DH=1.694$
 $Cp=.84$
 $T2=558.6$
 $Ps=29.23$
 $DP=0.8141$
 $CO2=2.1$
 $O2=18.4$
 $CO=0$
 $As=17.276$
 $Wt=0.0281$
 $?Redo \text{ from start}$
 $Wt=0.0281$
 $An=.000341$
 $Time: Minutes=57.5$
 $Time:Hours=0.95833$
 $Btu=1$

FLSPART

Company Name: Meyer Steel Drum

Location: Chicago

Test Number: 4

Test Date: 12/12/91

Source: Drum Reclamation Process Controlled by an Afterburner

Identification Number: 031 600 APY

Application Number: 91040073

PARTICULATE MATTER TEST

Concentration & Pollutant Mass Rate

$$Vwc = V1 \times 0.04707$$

$$Vwc = 49.6 \times 0.04707$$

$$Vwc = 2.33 \text{ scf}$$

$$VmStd = Y \times Vm \times (TsStd/Tm) \times (Pb + DH/13.6)/PsStd$$

$$VmStd = 1.102 \times 38.631 \times (528/527.7) \times (29.35556 + 1.634/13.6)/29.92$$

$$VmStd = 41.96 \text{ scf}$$

$$Bwo = Vwc/VmStd + Vwc$$

$$Bwo = 2.334672 / 41.96304 + 2.334672$$

$$BWO = 0.0527$$

$$\% H2O = 5.27$$

$$1-Bwo = 0.9473$$

$$Ms = Md(1-Bwo) + 18(Bwo)$$

$$Ms = 29.04 (0.9472959) + 18(5.270413E-02)$$

$$Ms = 28.46$$

$$Vs = 85.48 \times Cp \times (Ts/Ps \times Ms) \times Sq \times Rt \times Dp$$

$$Vs = 85.48 \times .84 \times (1001.3 / (29.35 \times 28.45815)) \times Sq \times Rt \times .7969$$

$$Vs = 62.65 \text{ feet per second}$$

$$Qs = As \times Vs \times 60$$

$$Qs = 17.276 \times 62.65019 \times 60$$

$$Qs = 64941 \text{ acfm}$$

$QsStd = Qs \times (Ps/PsStd) \times (TsStd/Ts) \times (1-Bwo)$
 $QsStd = 64940.67 \times (29.35/29.92) \times (529/1001.3) \times (1-5.270413E-02)$
 $QsStd = 31821 \text{ scfm}$

$Cs = (Wt \times 15.43)/VmStd$
 $Cs = (.0262 \times 15.43)/41.96304$
 $Cs = 0.0096 \text{ grains/scf}$

$PMRc = (Cs \times QsStd \times 60)/7000$
 $PMRc = (9.633859E-03 \times 31821.35 \times 60)/7000$
 $PMRc = 2.6277 \text{ pounds/hour}$

$PMRa = (Wt \times As)/(Time:Hours \times An \times 454)$
 $PMRa = (.0262 \times 17.276)/(1 \times .000341 \times 454)$
 $PMRa = 2.9237 \text{ pounds/hour}$

$I = (PMRa/PMRc) \times 100$
 $I = (2.92371 / 2.627678) \times 100$
 $I = 111.27 \%$

$Isokinetic \text{ Rate} = (VmStd \times As)/(An \times Minutes \times QsStd) \times 100$
 $Isokinetic \text{ Rate} = (41.96304 \times 17.276)/(.000341 \times 60 \times 31821.35) \times 100$
 $Isokinetic \text{ Rate} = 111.35 \%$

$Y=1.102$
 $Vm=38.631$
 $T1=67.7$
 $Pb=29.355555$
 $DH=1.634$
 $Cp=.84$
 $T2=541.3$
 $Ps=29.35$
 $DP=0.7969$
 ?Redo from start
 $DP=0.7969$
 $CO2=1.9$
 $O2=18.4$
 $CO=0$
 $As=17.276$
 $Wt=0.0262$
 $An=.000341$
 $Time: Minutes=60$
 $Time:Hours=1.0$
 $Btu=1$
 $FO=1$